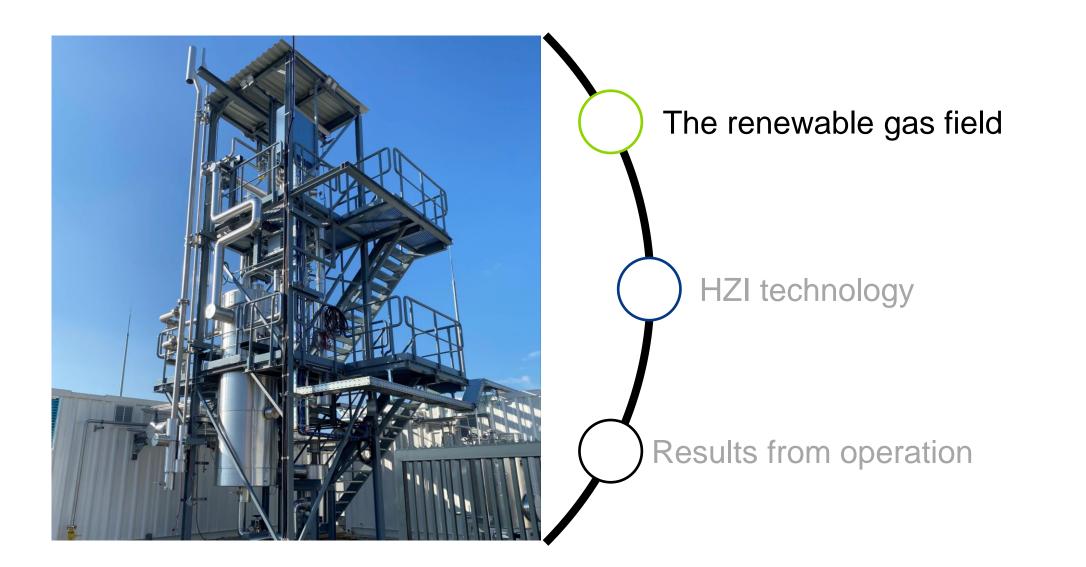
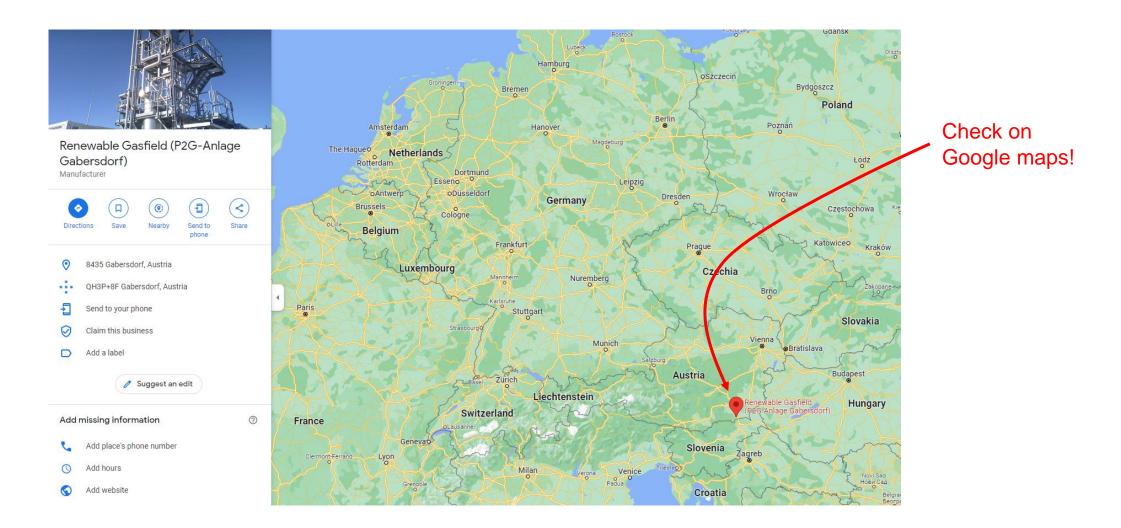


HZI Biogas methanation plant in Gabersdorf, Austria

E. Moioli – 27.03.2023



Where is Gabersdorf?



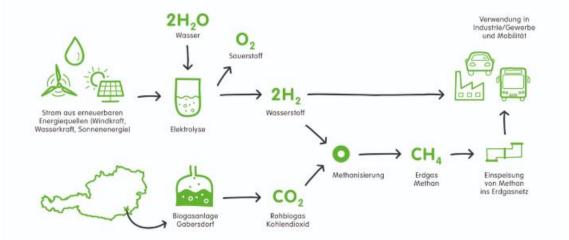
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Context of the plant

RENEWABLE GASFIELD

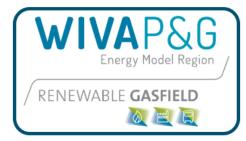
PROJECT DESCRIPTION ---

The decarbonization of the power supply and the shift from carbon-based energy sources to renewables lead to major changes in the energy economy to secure a long-term energy supply. Due to the high volatility of wind power and photovoltaics (PV) an increased energy storage demand is required. The existing Austrian natural gas grid offers an enormous storage potential. Green energy from wind power or PV is used in water electrolysis for hydrogen (H2) production and its following methanation of



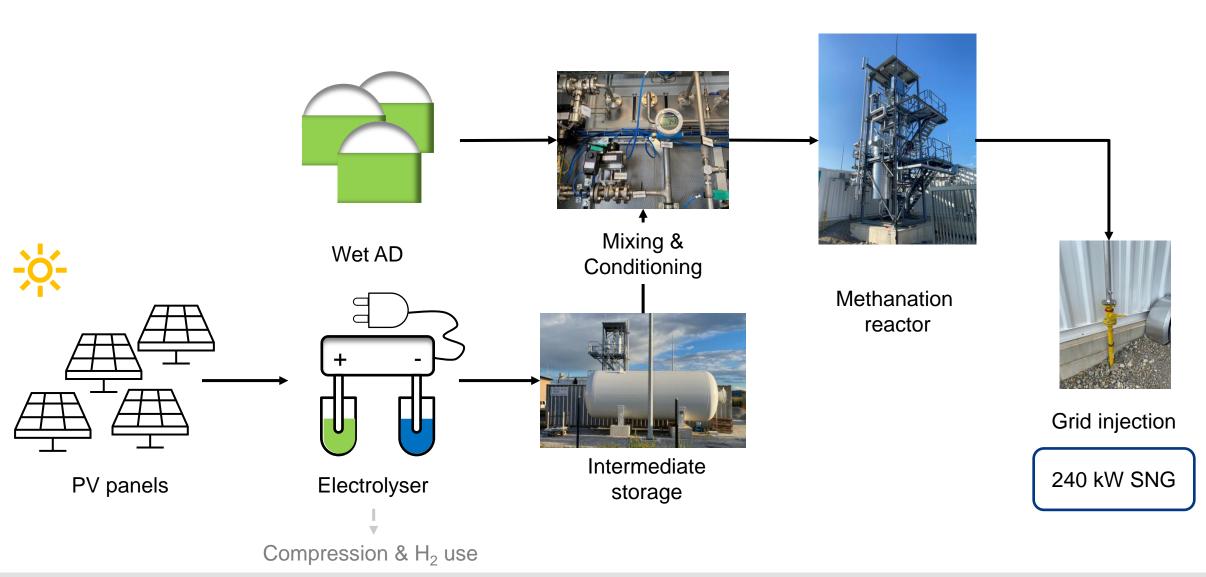
Project to realize a renewable gas field

- Biogas upgrading via methanation
- Electrolyser
- HZI methanation reactor





Gabersdorf plant at a glance



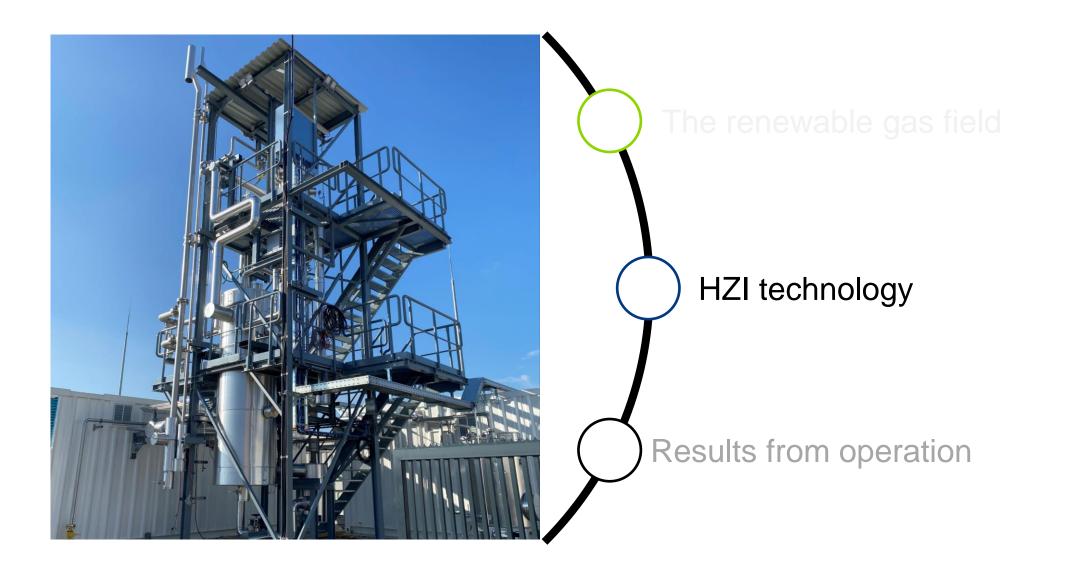
H₂ production side



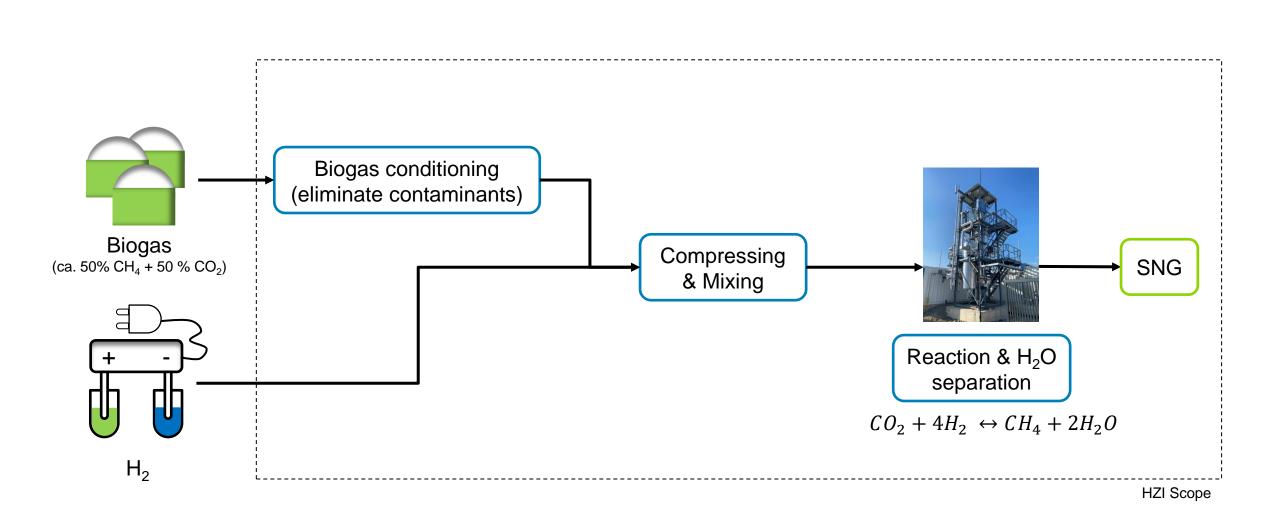
Biogas production



- Wet AD as source of CO₂
 - ca. 600-700 Nm³/h biogas production
 - Small amount of total CO₂ available is converted into methane
 - Currently, biogas is burnt in a combined heat and power plant (CHP)



Scope of the plant



Biogas conditioning (eliminate contaminants)

- Removal of sulphur and tars:
 - Activated carbons
 - CuO

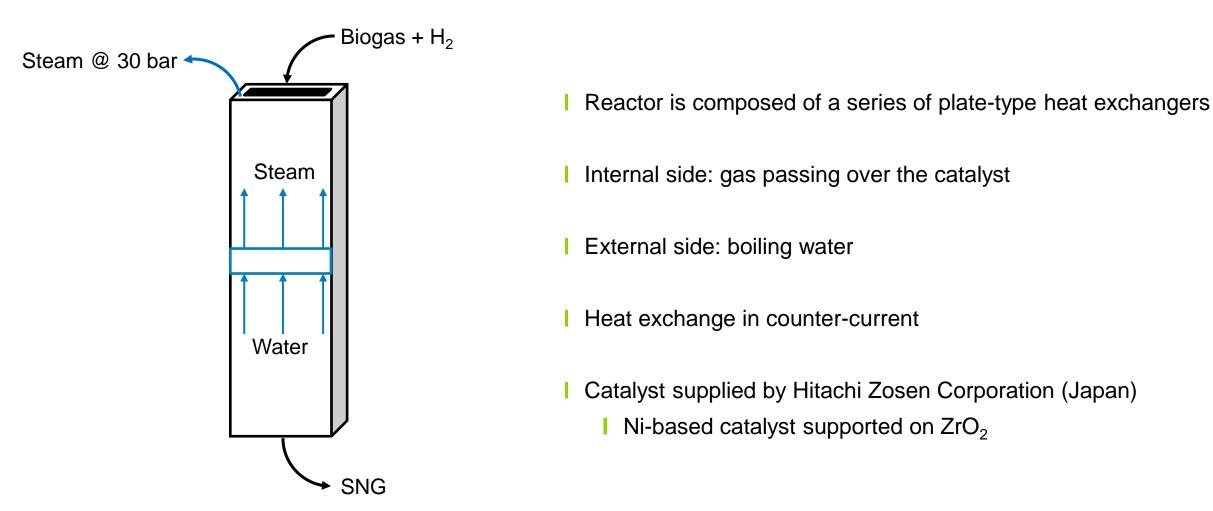
Compressing & Mixing

- Biogas is compressed to 10 bar
 - I Oil free compressor
 - 1 dedicated container for biogas compression
- In container also installed: Boiler feed water storage
 - Water circulation pump



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 - Oil free compressor
 - I dedicated container for biogas compression
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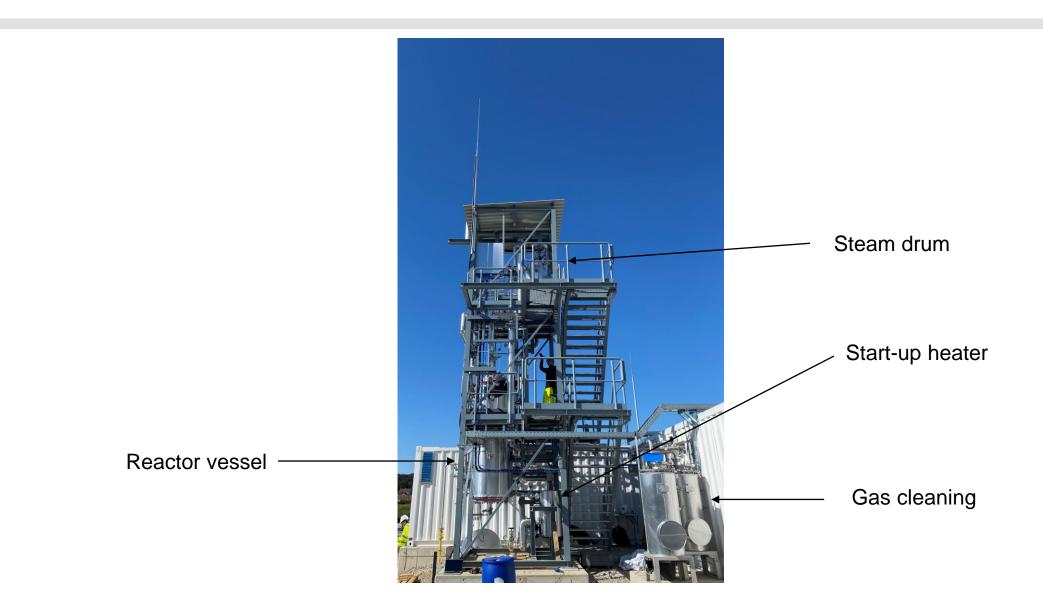
Reactor concept



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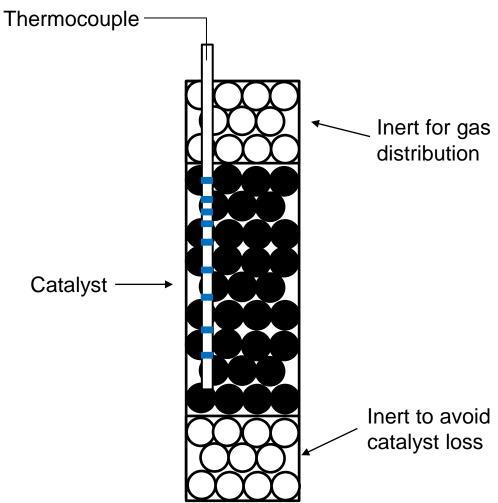
Methanation reactor



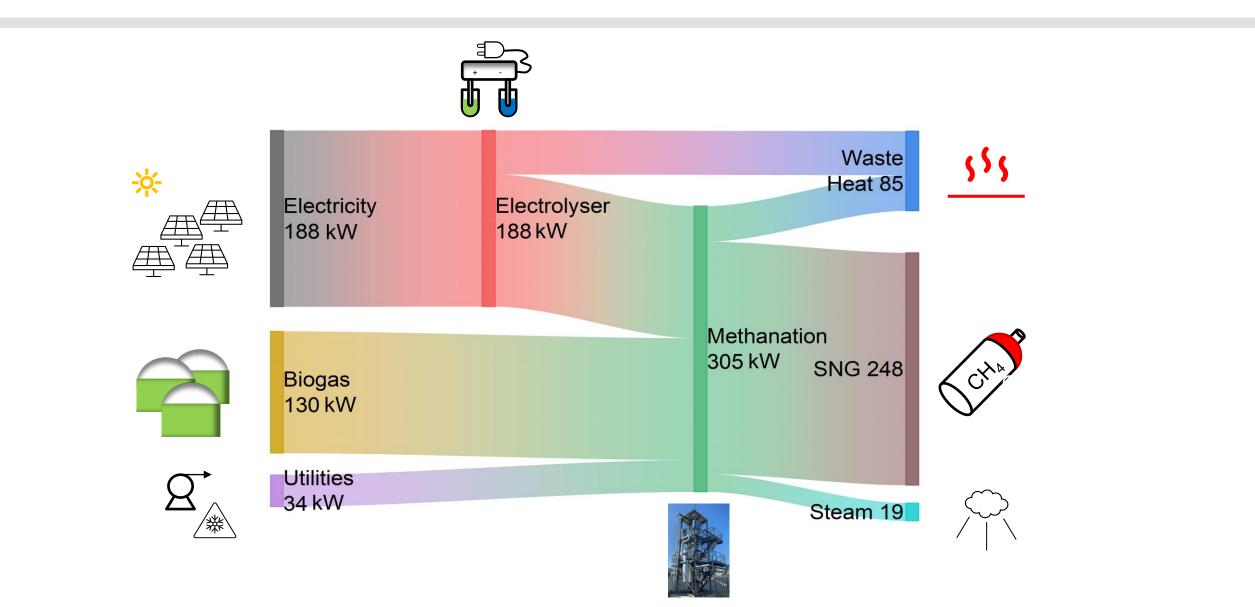
Inside the reactor

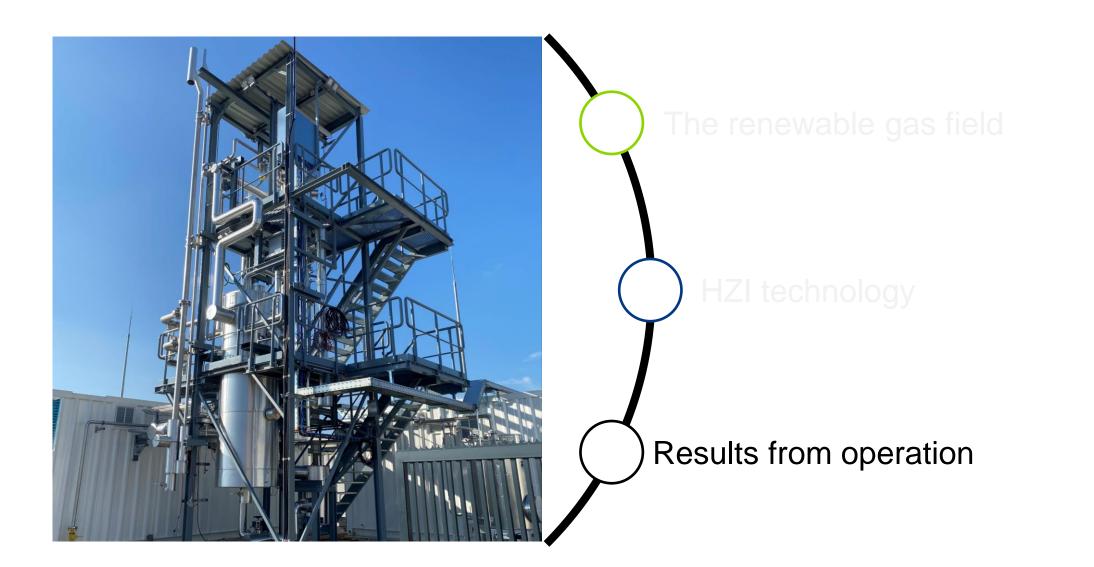
- Space between plates is filled with catalyst
- Inert layers are added to improve gas distribution and to stabilize the catalyst
- I Multipoint thermocouple is inserted to monitor the temperature inside the catalyst bed



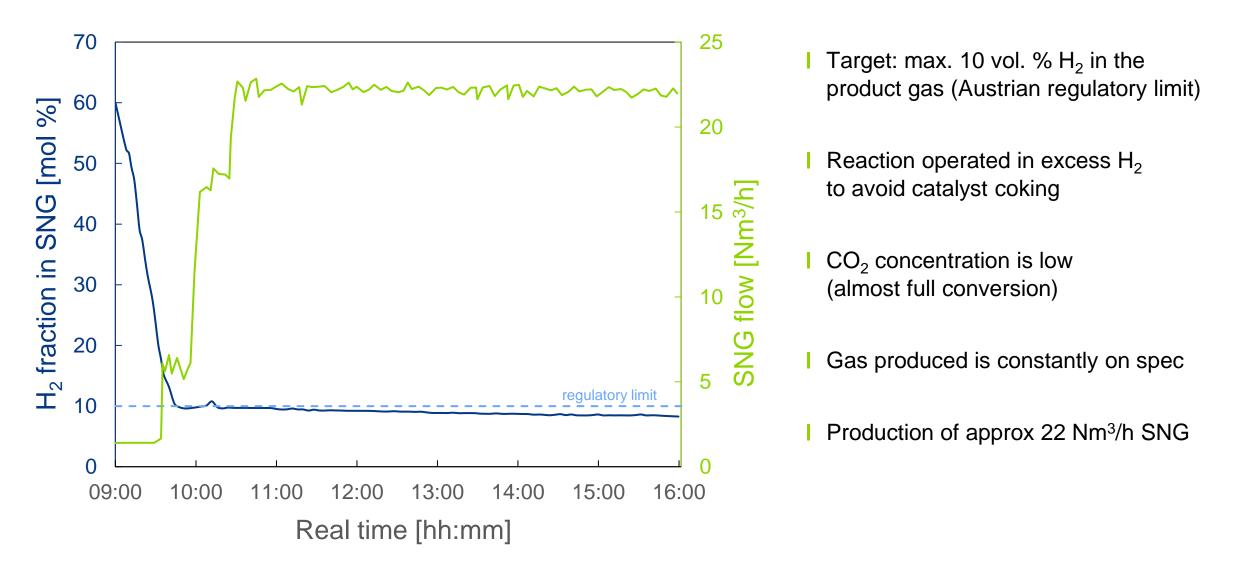


Energy balance



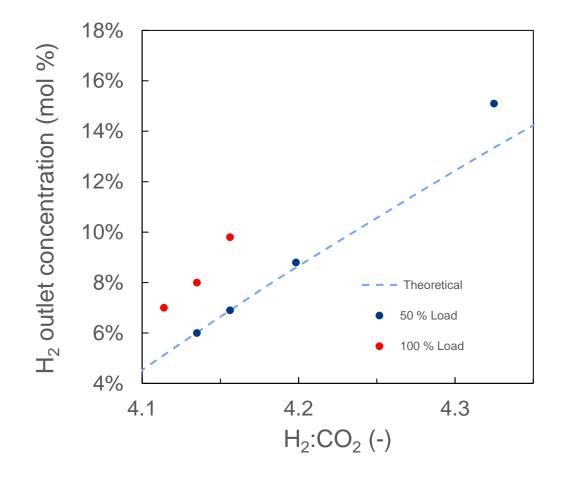


Long run results



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Effect of load/stoichiometry

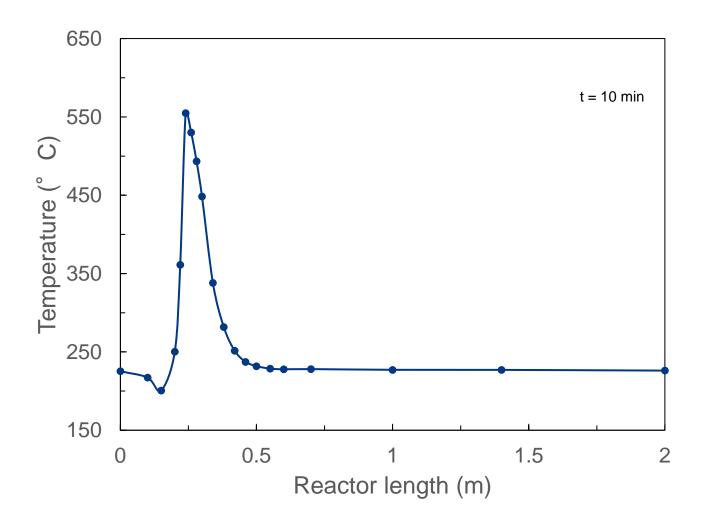


- At 50 % load, the results correspond to the stoichiometric limit
- At 100 % load, the measured value is ca. 2 % higher than theoretical limit
- I The specification is achieved in practically all the points investigated
- If H₂ conversion should be increased, it is possible to decrease the excess H₂
- In practical cases H₂ excess should be tailored to ensure catalyst durability and fulfilment of the specifications

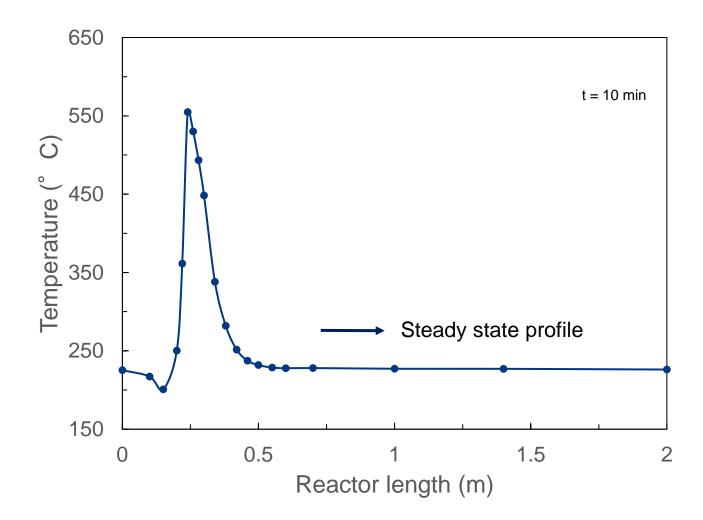
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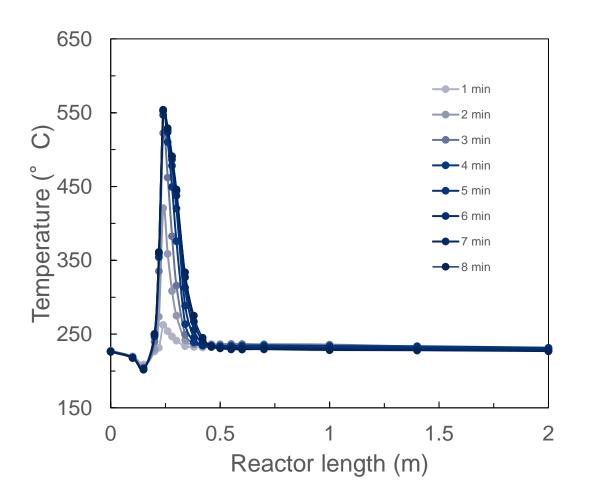
Reaction activation



Detailed analysis



Reaction activation at a glance

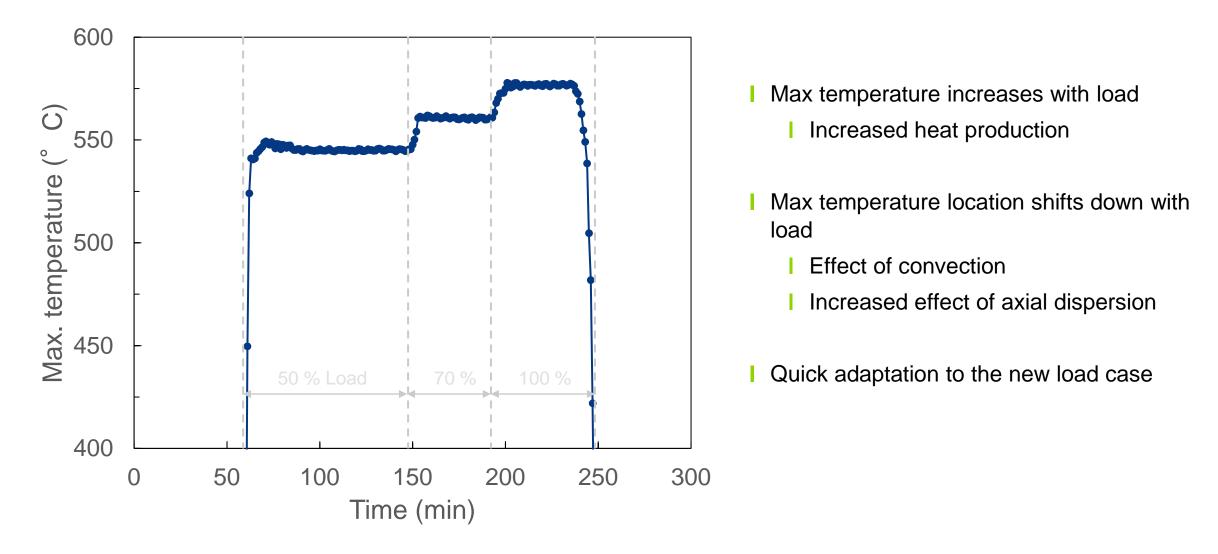


- Activation occurs in ca. 10 minutes
- I Hotspot formation is immediate
- Progressive increase of the hotspot area
- At steady state, hotspot area limited to ca. 25 % of the reactor length
- Max. temperature ca. 560 °C

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Evolution of max. temperature



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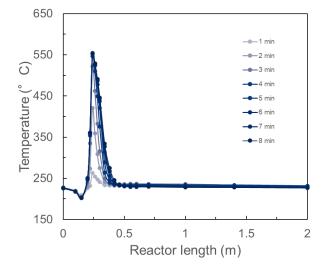
Conclusion dynamics of activation

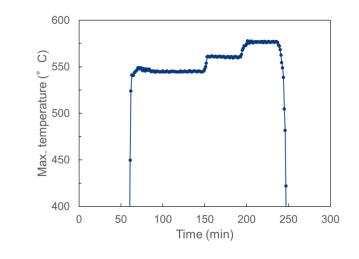
Quick activation from hot standby (ca. 10-15 min)

- Formation of cold spot at inlet
 - Convective flow of cold(er) gas
 - Larger extent with larger flow

- Hotspot position moves towards the end of the reactor with higher flow
 - Better heat transfer (convection)
 - Larger heat production

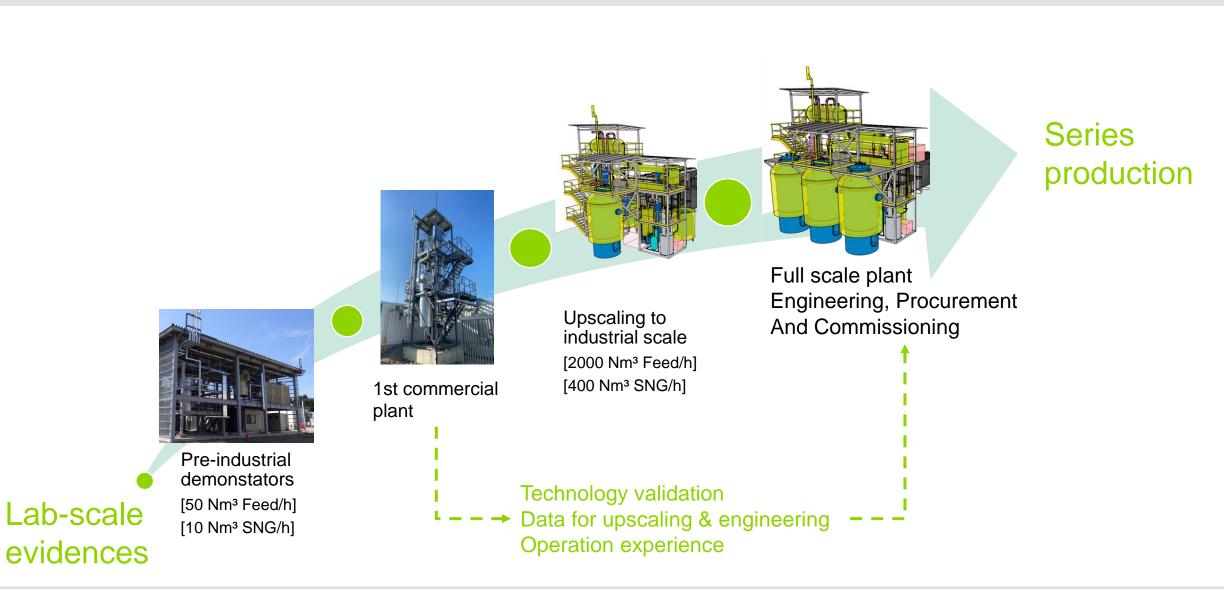
Maximal temperature remains in the safe range in all cases (< 600 $^{\circ}$ C)







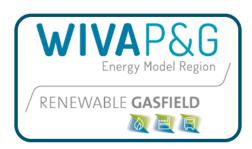
Outlook – where are we going?



Acknowledgments

Power-to-Gas teams from:

- Hitachi Zosen Inova AG
- Hitachi Zosen Inova Biomethan GmbH
- □ Hitachi Zosen Inova Etogas GmbH
- □ Hitachi Zosen Corporation



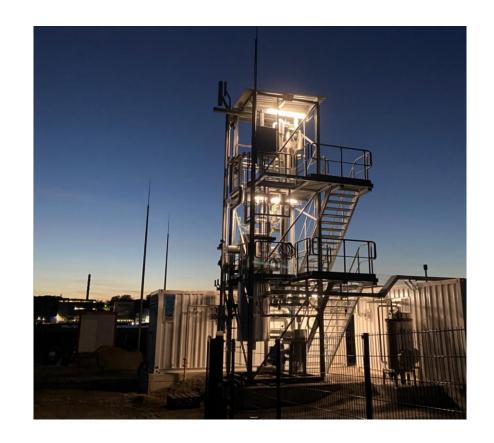


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Funding institution: FFG, KPC









Project number: 868849



Thank you for your attention!

